

Formulation of the thermohaline flow problem in FEFLOW

$$S \frac{\partial \varphi}{\partial t} + \text{div}(\mathbf{q}) = 0$$

$$\mathbf{q} = -\mathbf{K} \left(\mathbf{grad}(\varphi) + \frac{\rho_f - \rho_{0f}}{\rho_{0f}} \mathbf{u} \right)$$

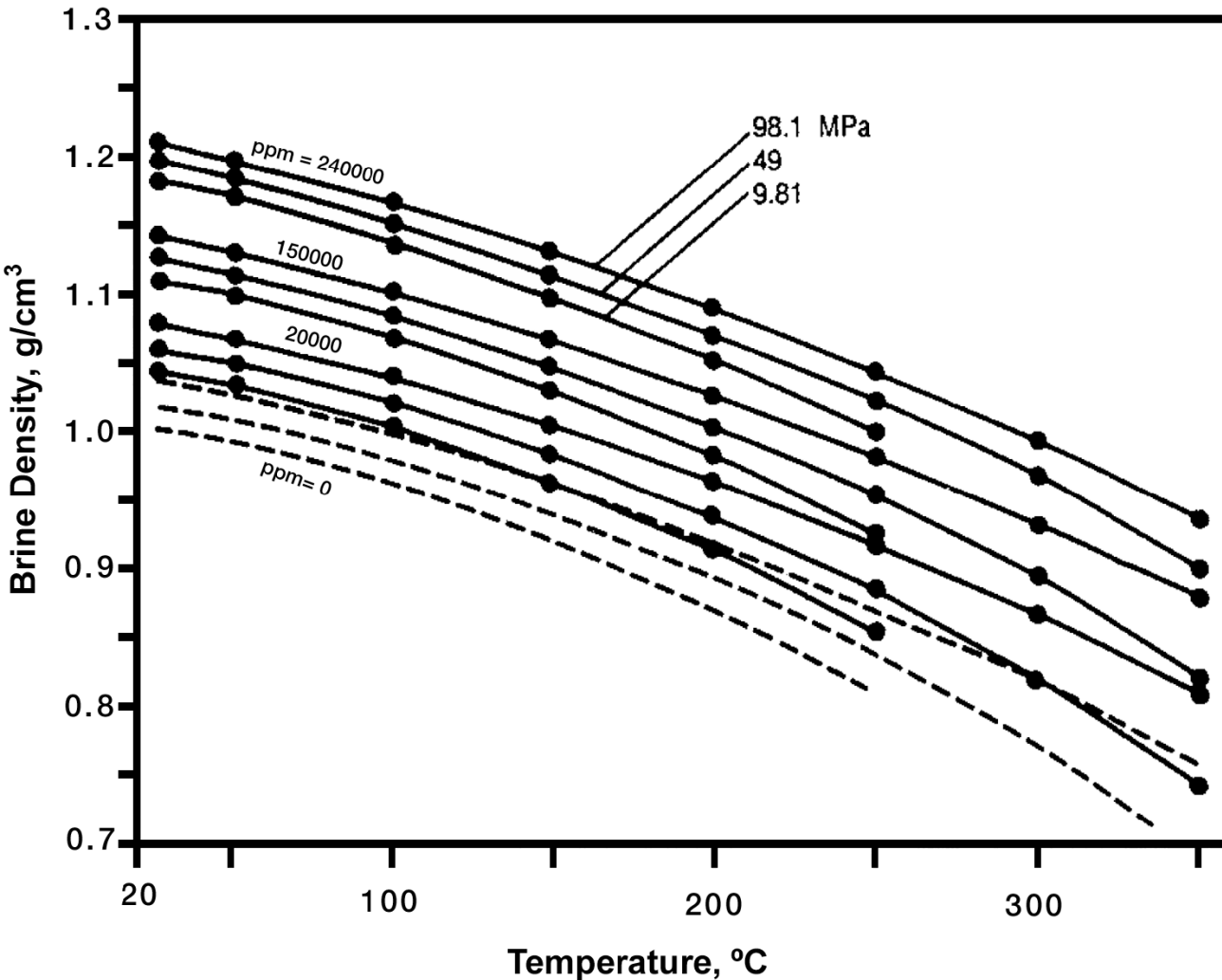
$$\mathbf{K} = \frac{\mathbf{k} \rho_{0f} g}{\mu_f(C, T)}$$
$$\rho_f = \rho_f(\varphi, T, C)$$

$$\phi \frac{\partial C}{\partial t} + \text{div}(\mathbf{q}C) - \text{div}(\mathbf{D} \mathbf{grad}(C)) = 0$$

$$\frac{\partial}{\partial t} \left((\phi \rho_f c_f + (1 - \phi) \rho_s c_s) T \right) + \text{div}(\rho_f c_f T \mathbf{q}) - \text{div}(\Lambda \mathbf{grad}(T)) = 0$$

Equations Of State in FEFLOW: brine density

$$\rho_f = \rho_{f0} \left(1 + \bar{\gamma}(p_f - p_{f0}) - \bar{\beta}(T_f - T_{f0}) + \bar{\alpha}(C_\alpha - C_{\alpha0}) \right)$$



Brinedensity as function of pressure and temperature

Equations Of State in FEFLOW: fluid viscosity

$$\mu_f(C, T) = \mu_0(1 + aC + bC^2 + cC^3 + dT(1 - e^{kC})) \quad a, b, c, d, k \text{ are constants}$$

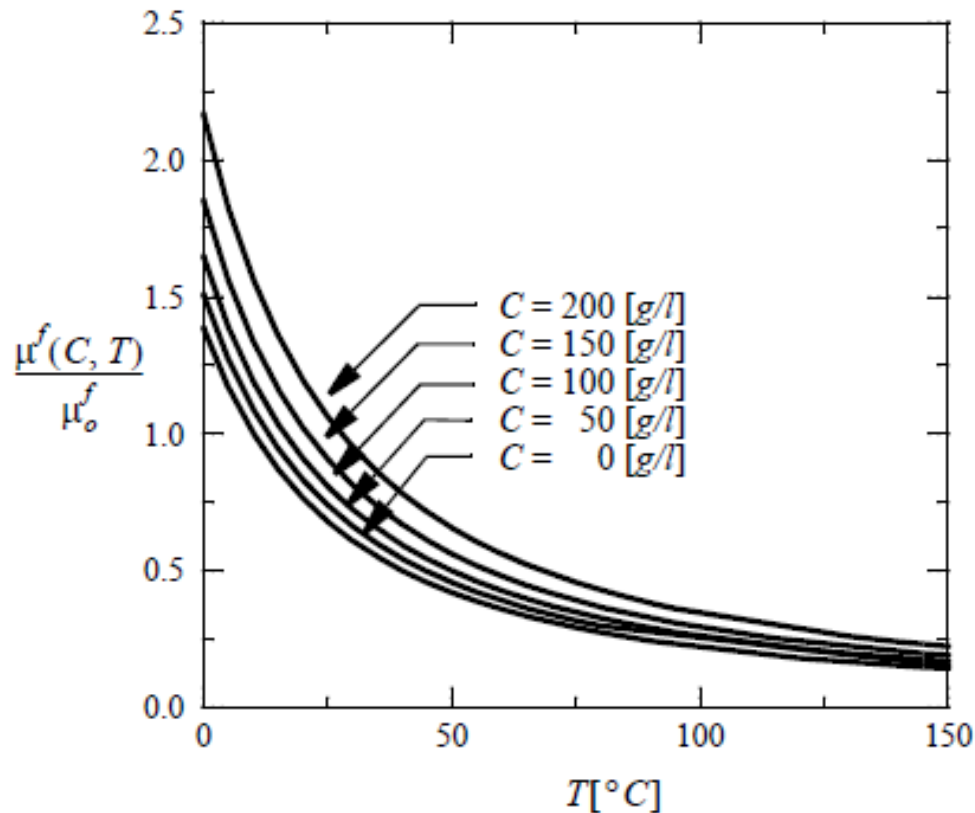
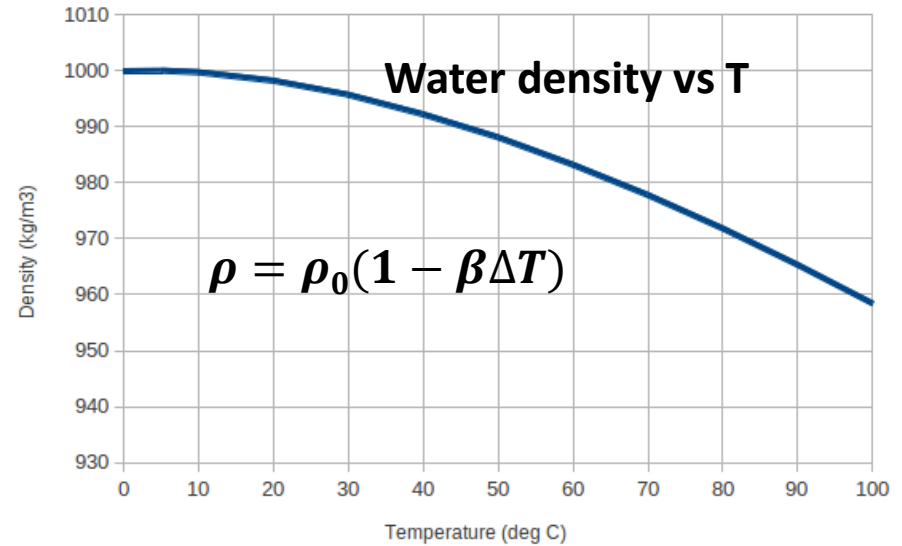
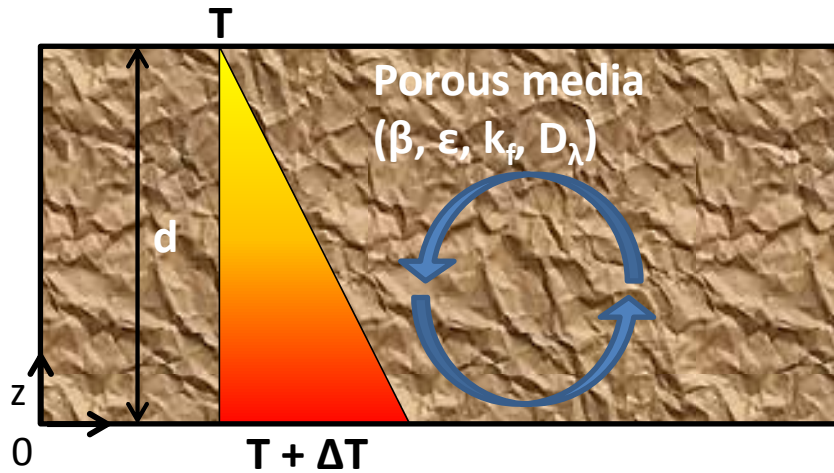


Figure 1.7 Relative viscosity μ^f/μ_o^f as function of temperature T [°C] and concentration C [g/l] with μ_o^f for the reference temperature of $T_o = 10$ °C and reference concentration of $C_o = 0$ (freshwater).

Thermal Rayleigh-Number (Ra_T) for an homogeneous porous media heated from below



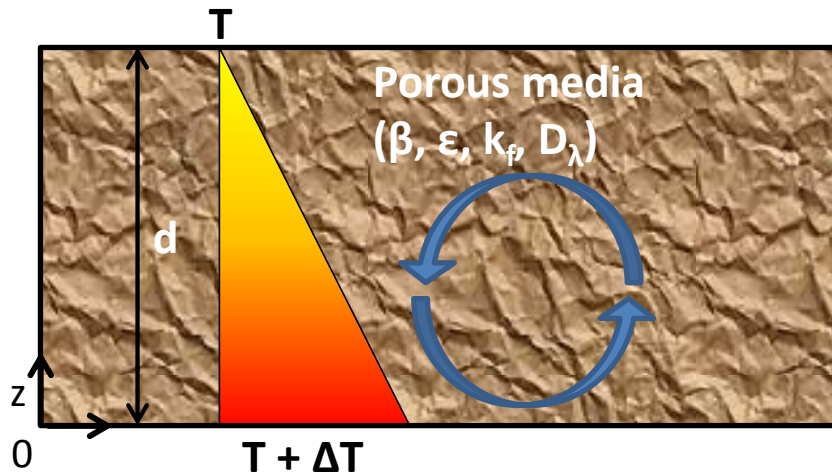
The Engineering ToolBox
www.EngineeringToolBox.com

The Rayleigh number(Ra) allows to predict the onset of convection:

$$Ra = \frac{\beta \Delta T k_f d}{D_\lambda}$$

β	Expansion coefficient	$[\Theta^{-1}]$
ΔT	temperature difference	$[\Theta]$
K_f	hydraulic conductivity	$[L^*T^{-1}]$
d	height	$[L]$
D_λ	Thermal diffusivity	$[L^2*T^{-1}]$

Thermal Rayleigh-Number (Ra_T) for an homogeneous porous media heated from below



$$Ra_T = \frac{\beta \cdot \Delta T \cdot k_f \cdot d}{D_\lambda}$$

$$D_\lambda = \frac{\Lambda}{\rho \cdot c_l} \quad [L^2 * T^{-1}]$$

$$\Lambda = \lambda_{cond} + \lambda_{disp} [M * L * T^{-3} * \Theta^{-1}]$$

ρ	Fluid density	$[M * L^{-3}]$
C	heat capacity	$[M * L^2 * T^{-2} * \Theta^{-1}]$
C_l	specific heat capacity	$[L^2 * T^{-2} * \Theta^{-1}]$
$\rho(c/[M])$	volumetric heat capacity	$[M * L^{-1} * T^{-2} * \Theta^{-1}]$
k_f	hydraulic conductivity	$[L * T^{-1}]$
β	expansion coefficient	$[\Theta^{-1}]$
ΔT	temperature difference	$[\Theta]$
d	length (height)	$[L]$
D_λ	Thermal Diffusivity tensor	$[L^2 * T^{-1}]$
Λ	hydrodynamic thermodispersion	$[M * L * T^{-3} * \Theta^{-1}]$
λ	thermal conductivity	$[M * L * T^{-3} * \Theta^{-1}]$
ε	Porosity	$[1]$

Critical Rayleigh-Numbers

2D homogenous medium / infinite porous medium

$$Ra_{\text{critical1}} = 4\pi^2 = \mathbf{39,48}$$

$$Ra_{\text{critical2}} = \mathbf{240-300}$$

$$Ra < Ra_{\text{critical1}}$$

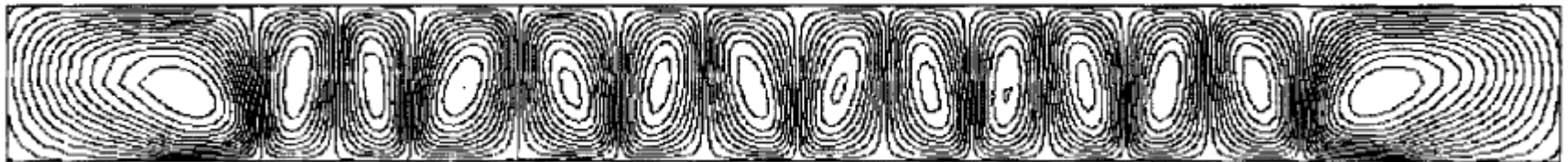
→ pure conduction

$$Ra_{\text{critical1}} < Ra < (240-300)$$

→ stable convergent solution develops
and various steady-state flows occur

$$Ra > Ra_{\text{critical2}}$$

→ convection regime is unstable



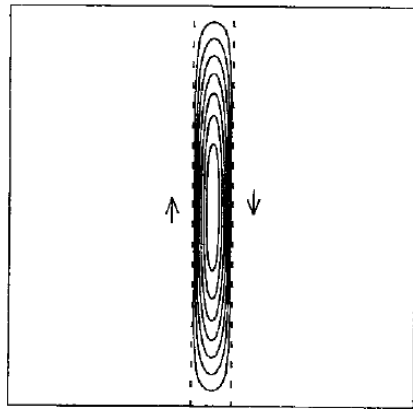
Streamlines for a 2D convective problem (Diersch, 2002)

Critical Rayleigh-Numbers

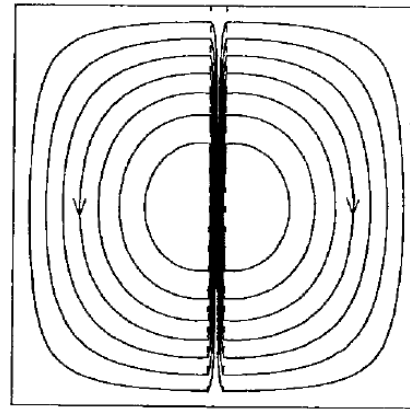
Problem: nature is heterogeneous

→ $Ra_{critical} = 4\pi^2$ is not indicative of the onset of convection for heterogeneous media

In a fault surrounded by an impervious rock,
the onset of convection occurs for much higher Rayleigh!



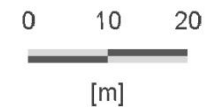
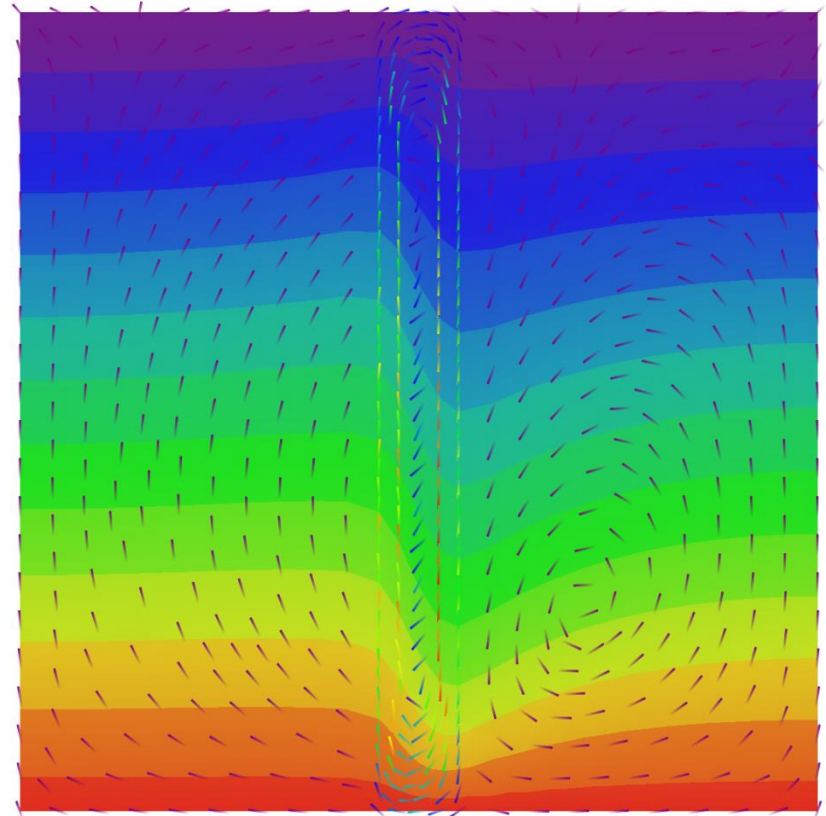
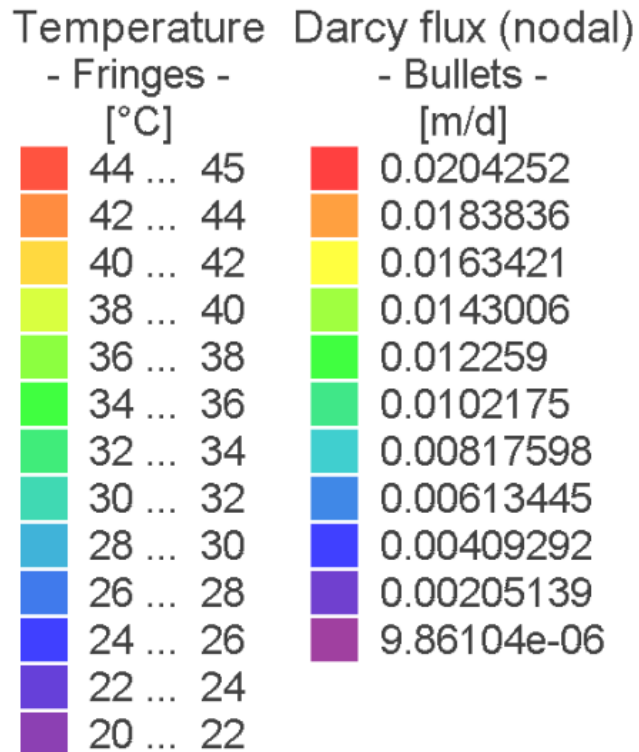
$Ra_{fault} = 1054$
 $Ra_{surrounding} = 10$



$Ra_{fault} = 2625$
 $Ra_{surrounding} = 26$

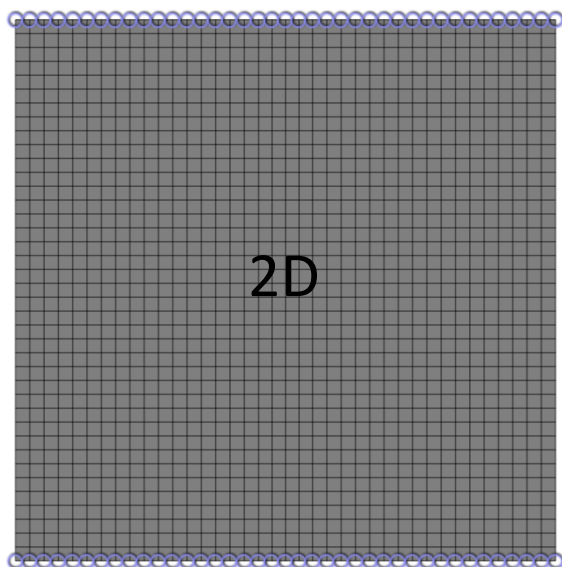
Streamline patterns (McKibbin,1986)

McKibbin example nicely reproduced



18.8 [d]

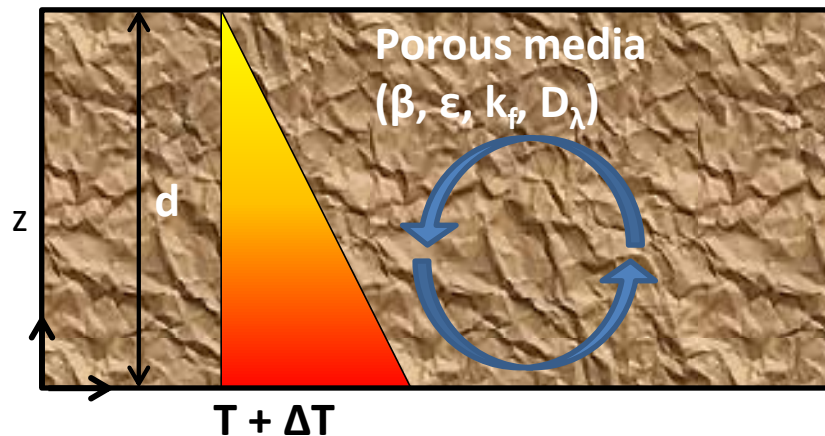
FEFLOW Exercise



When will convection occur?

Change β or ΔT or k_f

Compare with Ra theory



- **1st-kind (Dirichlet) heat transport BC**
→ *fixed temperature at the top and the bottom*
- **1st-kind (Dirichlet) flow BC**
→ *fixed Hydraulic-Head in the upper left and right corner as a reference value*
- (the surrounding bounds are set as No-Flow-BC by default)

Additional slides

Fault and surrounding rock

$$Ra_{Tcritical}^{3D} = \frac{\left[\left(\frac{H_3}{H_1} \right)^2 + \left(\frac{H_3}{H_2} \right)^2 + 1 \right]^2 \pi^2}{\left(\frac{H_3}{H_1} \right)^2 + \left(\frac{H_3}{H_2} \right)^2}$$

$$H_3/H_1 \ll 1$$

$$H_{3(\text{height})} \ll H_{1(\text{length})}$$

$$Ra_{Tcritical}^{2D} = \frac{\left[\left(1 + \left(\frac{H_3}{H_2} \right)^2 \right)^2 \pi^2}{\left(\frac{H_3}{H_2} \right)^2}$$

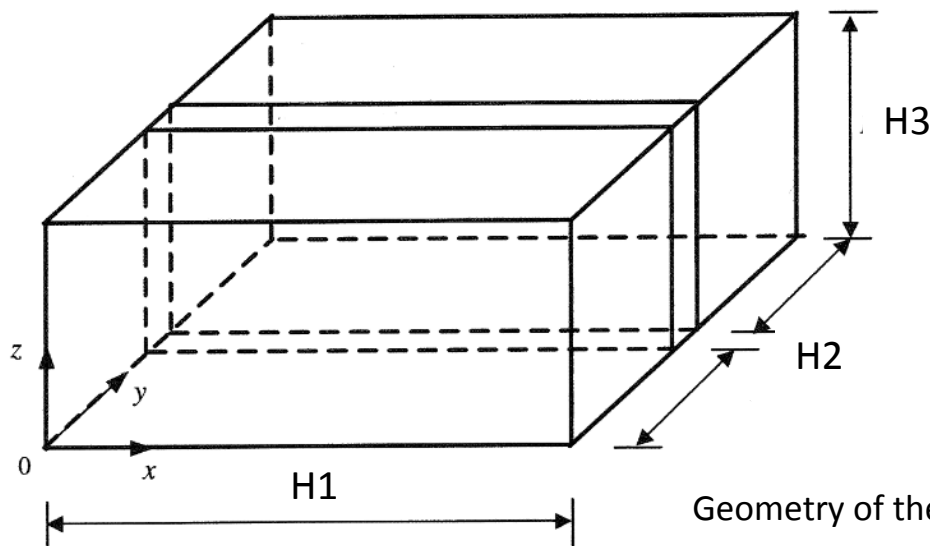
$$H_3/H_2 \gg 1$$

$$H_{3(\text{height})} \gg H_{2(\text{width})}$$

$$H_1/H_2 \gg 1$$

$$H_{1(\text{length})} \gg H_{2(\text{width})}$$

if H_1 tends to infinity: $Ra_{critical}^{2D} = Ra_{critical}^{3D}$

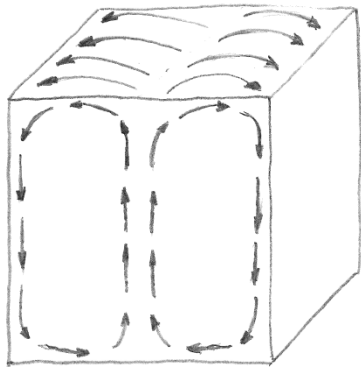


Geometry of the problem (Zhao et al. 2006)

Same geometry - different Rayleigh-Numbers

$$Ra_{\text{critical}} = 4\pi^2 = 39,5$$

$Ra_T = 70$



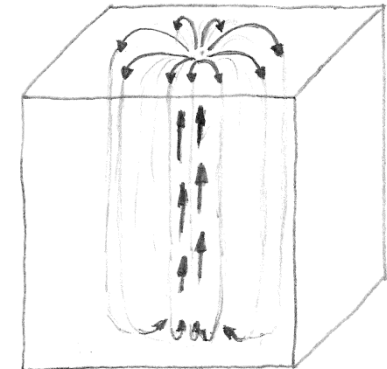
- two stable convection cells
- like in 2D

$Ra_T = 330$



- unstable flow pattern
- no symmetry
- ≠ 2D

$Ra_T = 1200$

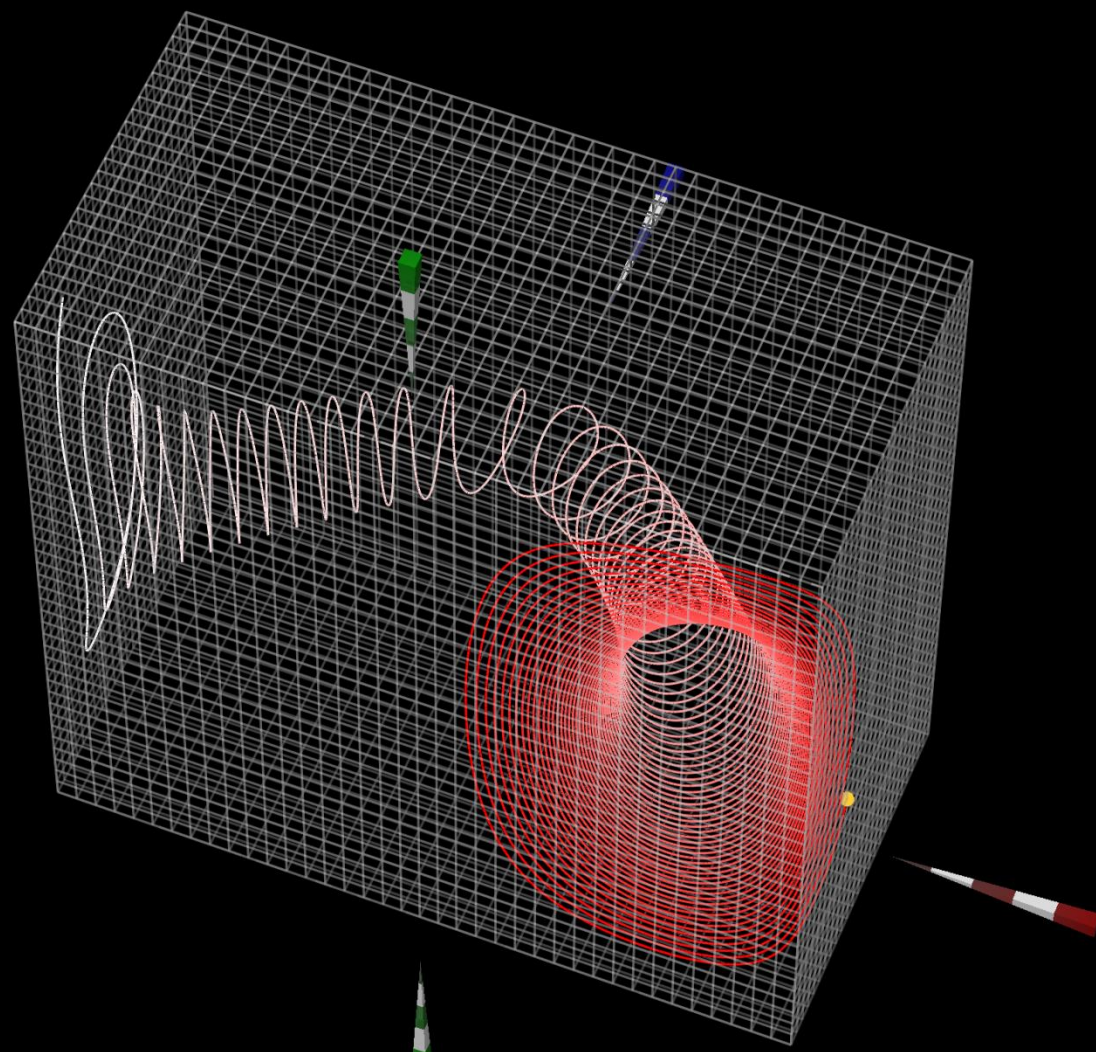
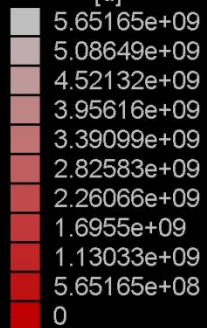


- radial symmetric convection cell
- only for a short time stable

Travel time, forward streamlines
seeded @Current Node Selection

- Traces -

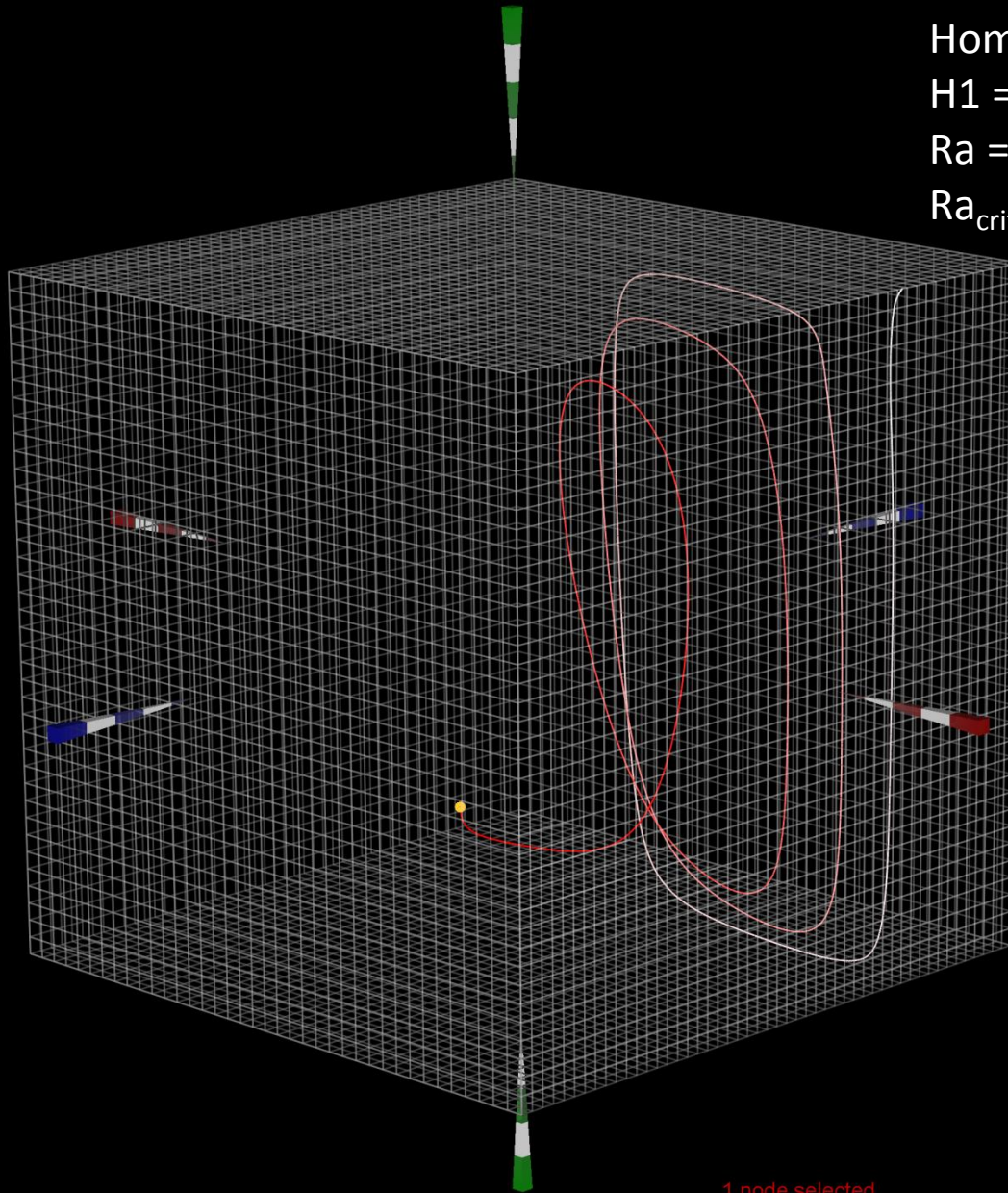
[d]



Travel time, forward streamlines
seeded @Current Node Selection

- Traces -

[d]



Homogenous cube

$H1 = H2 = H3 = 100 \text{ m}$

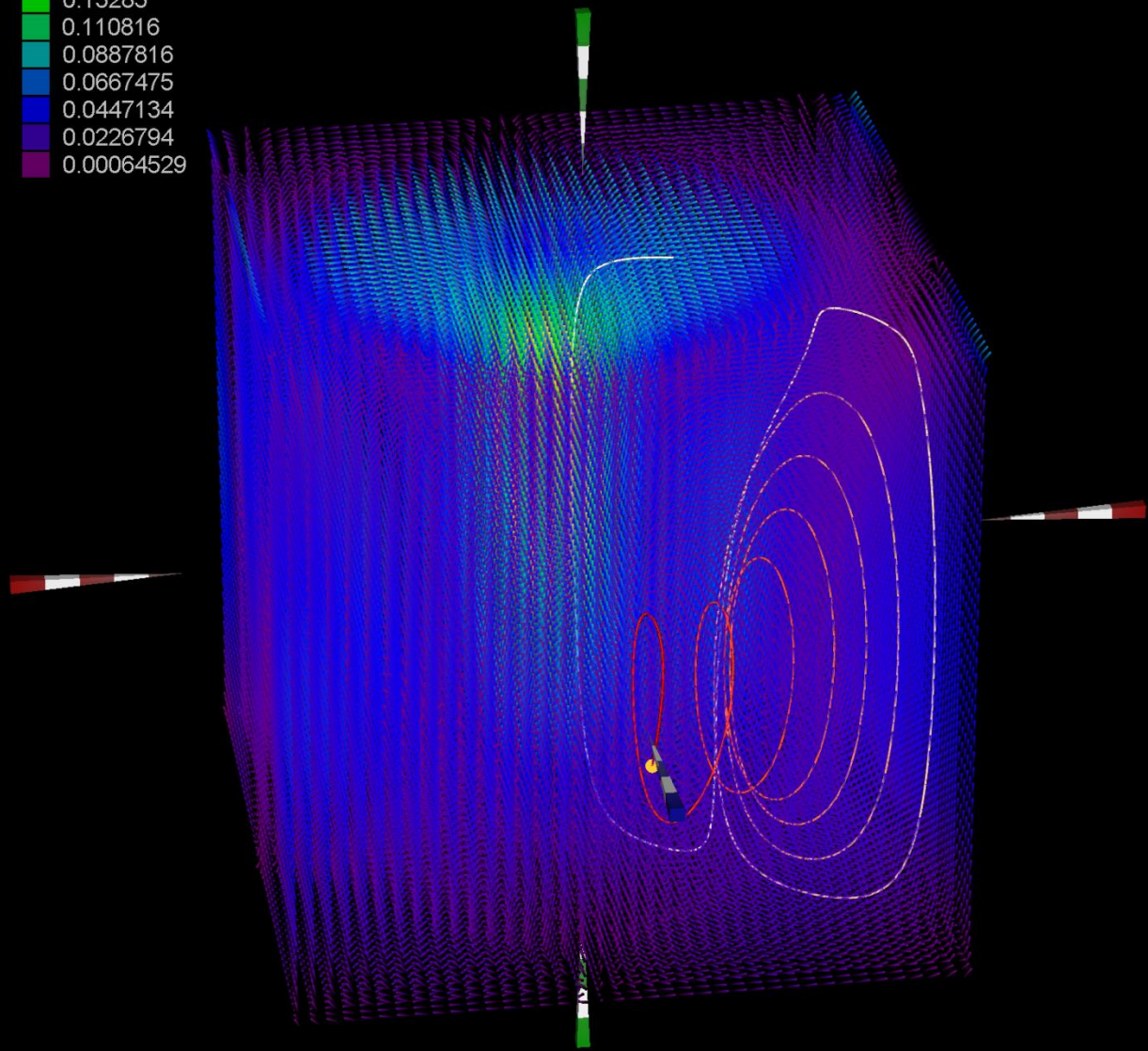
$Ra = 330$

$Ra_{\text{critical } 3D} = 4,5\pi^2 = 44,4$

1 node selected
18000 [d]

Travel time, forward streamlines Darcy flux (nodal)
 seeded @Current Node Selection - Bullets -
 - Traces - [m/d]

[d]	0.220986
12820	0.198952
11538	0.176918
10256	0.154884
8974	0.13285
7692	0.110816
6410	0.0887816
5128	0.0667475
3846	0.0447134
2564	0.0226794
1282	0.00064529
0	



1 node selected
 1802.68 [d]



Same Rayleigh-Number – different geometry

2D
 $Ra_T = 1200$

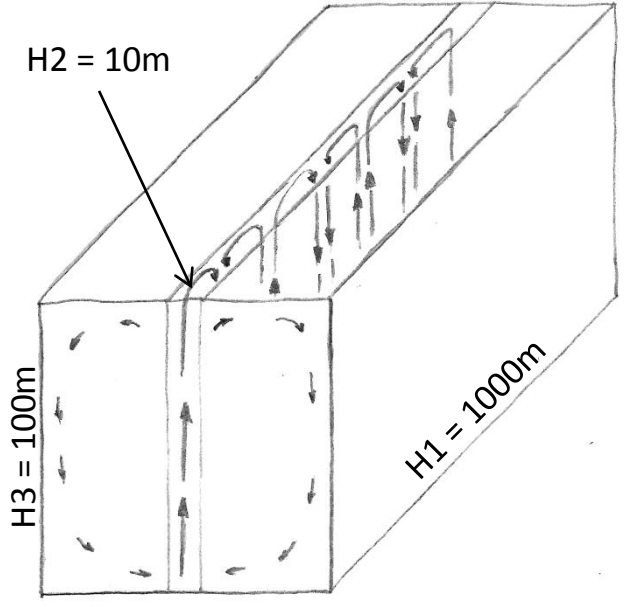
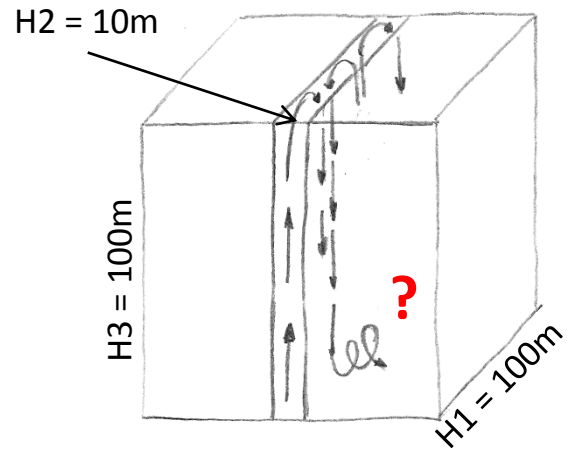
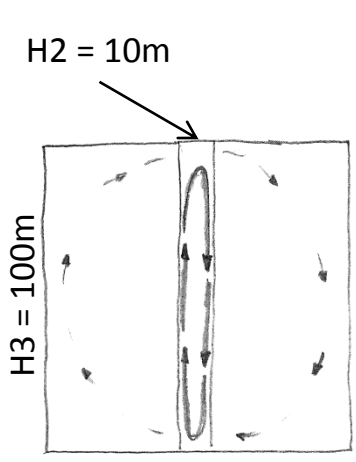
3D
 $Ra_T = 1200$
 $H1 = 100\text{ m}$

3D
 $Ra_T = 1200$
 $H1 = 1000\text{ m}$

$Ra_{critical}^{2D} = 1006$

$Ra_{critical}^{2D} = 1006$
 $Ra_{critical}^{3D} = 1016$

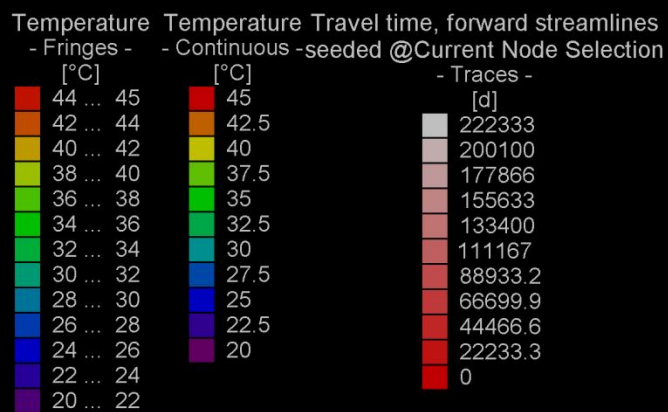
$Ra_{critical}^{2D} = 1006$
 $Ra_{critical}^{3D} = 1006$



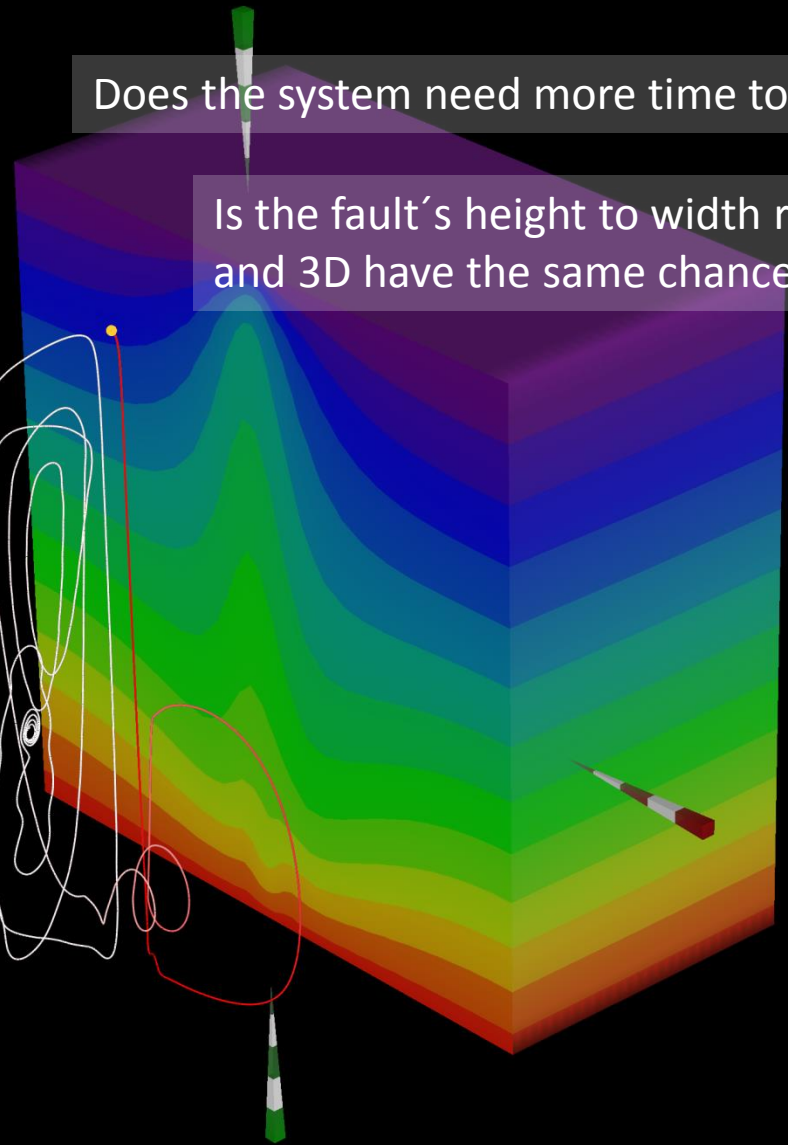
- different mode of convection compared to the 3D case

$Ra_{critical}^{3D} \neq Ra_{critical}^{2D}$
BUT: 3D and 2D have the same chance to develop, if the height to width ratio is small

$Ra_{critical}^{3D} = Ra_{critical}^{2D}$
→ $H1$ tends to infinity



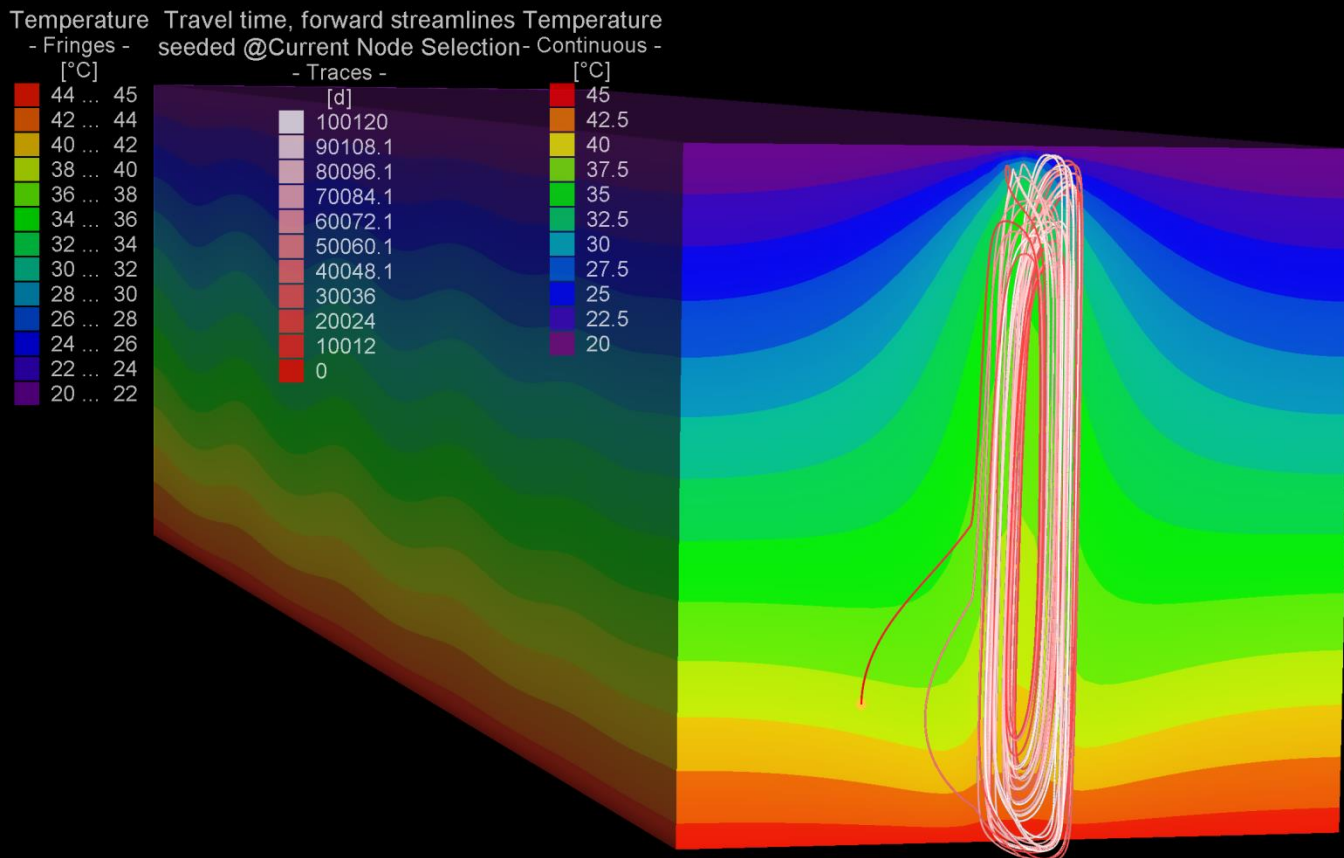
$H1 = H3 = 100\text{m}$ (cube)
 $H2 = 10\text{m}$ fault
 $Ra = 1200$
 $Ra_{critical}^{3D} = 1016$
 $Ra_{critical}^{2D} \neq Ra_{critical}^{3D}$



Does the system need more time to reach the 3D state?

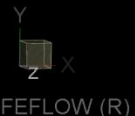
Is the fault's height to width ratio too small, so 2D and 3D have the same chance to occur?





$H1 = 1000 \text{ m (length)}$
 $H2 = 10 \text{ m (fault)}$
 $H3 = 100 \text{ m (height)}$
 $Ra = 1200$
 $Ra_{critical}^{3D} = 1016$
 $Ra_{critical}^{2D} = 1016$
 $Ra_{critical}^{2D} = Ra_{critical}^{3D}$
Cause $H1$ tends to infinity

Slender typ of convection zhao



1 node selected
37763.1 [d]